The paper presents a new criterion equation for calculating the Nusselt number for heat transport by natural convection from different numbers of cylindrical surfaces of heating sources. Horizontal cylindrical surfaces are situated one above the other and each of them is independently electrically heated by constant power output of Joule heating. Correlation relationships were derived on the basis of tens of measurements of heat outputs of the system of electrically heated horizontal cylindrical surfaces in a thermostatic chamber under defined conditions. The number of cylindrical surfaces, their distance and heat output to the horizontal cylinder varied during measurements. The derived criterion equation is significantly simpler compared to equations corrected by polynomial regression.

Keywords: Natural convection, cylindrical surfaces one above the other, criterial equations.
To compute the Nusselt number for a long horizontal cylinder and a wide range of the Rayleigh number, the relation according to Churchill-Chu [4] is recommended:

\[ Nu = 0.60 + \left( \frac{0.387 \cdot Ra^{1/6}}{1 + (0.559/Pr)^{1/3}} \right)^2 \]

for \( 10^4 < Ra < 10^{12} \) (2)

where:

- \( Pr \) is the Prandtl number.

For the range \( Ra \) of the following relation holds for natural convection:

\[ Nu = 0.36 + \left( \frac{0.518Ra^{1/4}}{1 + (0.559/Pr)^{1/3}} \right)^{1/2} \]

Past publications and research of natural convection from horizontal cylindrical heat transfer surfaces have not mentioned correlation relationships for the Nusselt number of the bundle of heat transfer surfaces which are most frequently used in heating and cooling technology and which would enable complex quantification of the total heat output of the bundle. The influence of pipe distance on the overall heat transfer in natural convection from the pipe bundle was analysed within the experiment by measurements of heat output of a model of a heating source consisting of 10 horizontal pipes having a diameter of 20 mm and length of 1000 mm [5].
An objective of analyses was to determine the impact of pipe distance on heat transfer from the pipe system and their impact on the overall heat output of the pipe bundle. The distances among the pipe walls were 0 mm (Fig. 3), 10 mm, 20 mm and 40 mm (Fig. 4). Measurements were done at temperature gradients 55 °C/45 °C, 75 °C/65 °C, 85 °C/75 °C, the ambient temperature of 20 °C. The measurement was compared with a CFD mathematical model of heat transport from the system of pipes situated one above the other.

An extensive set of numerical experiments in the field of heat transport by natural convection from oriented heat transfer surfaces was performed by Kapjor [6] and experiments were done by Annunziata D’Orazio [7]. From the gathered material Kapjor created a new criterion relation for the computation of the Nusselt number for natural convection from “n” horizontally arranged cylindrical surfaces situated one above the other by means of polynomial regression. In ANSYS Fluent code tens of heat transport simulations were performed from ten pipes having an outer diameter of 20 mm situated one above the other. The wall temperature was 30 °C, 45 °C, 60 °C, 75 °C, 90 °C, 105 °C and ambient temperature 20 °C. It was expected that the heat output in natural convection from “n” horizontal pipes situated one above the other is dependent on dimensionless spacing $H/D$ as well as on dimensionless variable $T_\infty/T_s$. At approximation the least square method for the function of two variables was used. Approximation polynomial regressions of higher orders ($n > 5$) were computed from functional dependencies of the Nusselt number of the bundle of horizontal pipes in ratio $H/D$ and $T_\infty/T_s$.

Analytical solutions and experiments show that heat transfer by natural convection from any surface depends on the surface geometry, on its orientation as well as on distribution of temperature on the surface and also on thermo physical characteristics of liquid.

Reference temperature, from which physical characteristics needed for computation are determined, is the average temperature of the boundary layer:

$$T_f = \frac{(T_s + T_\infty)}{2} \quad [°C].$$

The flow of liquid in natural convection can be unstable due to the occasionality of turbulence. This instability is caused by flow disturbances which gradually get stronger and laminar flow becomes turbulent. As already mentioned, the flow character in natural convection determines the criterion of the Rayleigh’s $Ra$.

3. Measurement and thermal analysis of horizontal heating pipes situated one above the other

The measurement of heat flows of the bundle of horizontal heat transfer surfaces was performed in a thermostatic chamber. During measurements, the temperature of the chamber inner walls was controlled so that the reference value of air temperature in the chamber, which was measured by Vernon resistance thermometer PT-100 DIN 1/5, would be stationary 20 ± 0.5°C.

The thermostatic chamber is controlled by Siemens Systematic S7-300. Visualization D2000 is programmed to the regulation system to visualise the situation in the thermostatic chamber. It provides a fully automated control of the chamber and helps to achieve equilibrium conditions at different measurement requirements within the range of measurability range.

Other experiments performed in the thermostatic chamber were measurements of thermal outputs from various systems of vertical arrangement of horizontal heated cylinders placed one above the other with an objective to design a new form of criterion equation for the computation of the Nusselt number of such a bundle. To obtain output and thermal parameters necessary for the creation of a new criterion relationship on the basis of which it would be possible to quantify the thermal output from “n” vertically arranged horizontal heated cylinders placed one above the other in natural convection, the measurements in the thermostatic chamber together with simulation analyses in ANSYS Fluent were performed gradually on three, five and ten horizontal cylinders situated one above the other. The principle and method of measurement were similar to those used for measurement and analysis of thermal output from one heated horizontal cylinder.

The measurement in thermostatic chamber consisted of the measurement of thermal and output parameters from three, five and ten electrically heated horizontal cylinders placed one above the other.

Ten, five and three heated cylinders were horizontally fixed on the stand in the thermostatic chamber (Fig. 5). During
measurement each cylinder was heated by the same electric output. The distance among individual cylinders gradually changed from 20 mm to 100 mm, with a step of 20 mm. The changing distance was defined by ratio $H/D$. Ratio $H/D$ represents a dimensionless distance among the cylinders (Fig. 6). The temperatures, the cylinders achieved after the supplied equal electric output, were measured.

As obvious from the values of individual measurements shown in the previous tables, the change of distance among individual cylinders results in outstanding change of surface temperatures of horizontal heated cylinders situated one above the other. When the distance among cylinders is 20 mm and 40 mm (ratio $H/D=1$ and $H/D=2$), the surface temperatures of the cylinders increase. This growth of temperature is caused by the fact that a thermal field is formed in the vicinity of the cylinder, which influences the cylinder placed above; thus in the vicinity of the cylinder placed above a thermal field with a higher temperature is formed, which causes the increase of its surface temperature at the constant electric input. Changing the ratio $H/D=3$, at which the distance among individual cylinder gets the value of 60 mm, the growth of the surface temperature is lower as there is no more significant impact on the individual cylinders and the surface temperatures of cylinders do not tend to increase. From the values of surface temperatures of cylinders placed at the distance of 100 mm it is obvious that there is no influence of thermal fields from the heated cylinders situated above them. The heated cylinders thus obtain temperatures corresponding to the values which were recorded when measuring one heated cylinder.

Generated thermal fields near the individual bundles of cylinders that originate in heat transfer from their surfaces to environment and their interaction result in the already mentioned growth of surface temperature of individual cylinders. This phenomenon can be better seen in Fig. 7 which shows chosen visualisations of thermal fields gathered from simulation analyses from ANSYS Fluent around three, five and ten heater horizontal cylinders situated one above the other.
Having logarithmized equation (5), it obtains the form (6)

$$
\log y = \log b_0 + b_1 \log x_1 + b_2 \log x_2 + b_3 \log x_3 + b_4 \log x_4.
$$

(6)

or (7)

$$
z = a_0 + b_1 y_1 + b_2 y_2 + b_3 y_3 + b_4 y_4.
$$

(7)

where the form is more suitable for the multi parametric linear regression. In its application various physical and geometric parameters were used as parameters $X_1, X_2, X_3$ and $X_4$.

The regression constant $b_0$ and regression coefficients $b_1 - b_4$ were obtained through specific functions for multi parametric regression in a table processor MICROSOFT EXCEL. The values of standard deviation $\sigma$ and correlation index $R$ were also set. The standard deviation simply gives the average difference between a computed and real value of the Nusselt number. The reliability...
of computed results obtained through correlation is given by the value of correlation index $R$. If this value exceeds 0.7, the results are generally acceptable; if this value exceeds 0.8, the results are good; if this value is higher than 0.9, the results are excellent.

After the analysis of the achieved results and their consequent processing we came to conclusion that the value of the Nusselt number from “n” vertically arranged horizontal pipes placed one above the other is mainly dependent on the changing distance among individual pipes, that is, on a dimensionless parameter, on the ratio $H/D$, on the number of heating pipes $n$, and also on the change of individual pipes situated one above the other. This change of surface temperatures is characterised by the average value of temperature difference $\Delta t_{str}$ obtained from all the heating pipes. The values $\Delta t_{str}$ are obtained from individual types of arrangements, from bundles of three, five and ten heating pipes. The ratio $(Pr/Prs)$ contains the influence of temperature taken on the first pipe wall on the heat transfer from the bundle of pipes in which the value $Pr$ was determined from ambient parameters and the value $Prs$ from the temperature of the first bottom pipe wall.

Owing to heat transfer by natural convection, the determining parameter was the criterion number $Ra = Gr.Pr$ whose values were computed similarly as in the case of natural convection from one pipe at $Ra = Gr.Pr < 10^6$.

The multiple linear regression was done for two types of obtained values:
- For values obtained from simulation computations in ANSYS Fluent,
- For values obtained from experimental measurements in the thermostatic chamber.

From the values obtained from simulation computations in ANSYS Fluent, we processed data by the multiple regression in Microsoft Excel. On their basis we created the equation which, having been de-logarithmized, gained the form

$$ Nu = 32.25 \cdot (H/D)^{0.16} \cdot n^{-0.03} \cdot Ra^{-0.27} \cdot (Pr/Prs)^{0.955}. $$

Figures 8a - 8d show comparison of values of the Nusselt number computed according to the obtained equation (8) with the values computed from simulation results for individual bundles of pipes.

In a similar way we did computation from the values obtained from measurements on experimental device in the thermostatic chamber. The computation was done in Microsoft Excel through the multiple linear regression.
The resultant criterion equation for natural convection from the bundle of pipes has the form

\[ Nu = 4.705 \cdot (H/D)^{0.14} \cdot n^{-0.02} \cdot Ra^{-0.03} \cdot (Pr/Pr)^{0.29}. \quad (9) \]

For the constant \( b_0 \), regression coefficients \( b_1 - b_5 \), standard deviation \( \sigma \) and correlation index \( R \) following values hold:

<table>
<thead>
<tr>
<th>( b_0 )</th>
<th>( b_1 )</th>
<th>( b_2 )</th>
<th>( b_3 )</th>
<th>( b_4 )</th>
<th>( R )</th>
<th>( S )</th>
</tr>
</thead>
<tbody>
<tr>
<td>4.705</td>
<td>0.14</td>
<td>-0.02</td>
<td>-0.03</td>
<td>-29</td>
<td>0.958</td>
<td>0.0117</td>
</tr>
</tbody>
</table>

Figures 9a - 9d show comparison of values of the Nusselt number computed according to the obtained equation (9) with the values computed from measured results for individual bundles of pipes.

5. Conclusion

From the performed analyses follows that the criterion equation for a bundle of horizontal pipes regularly situated vertically one above the other, proposed on the basis of a set of measured data shows a better correlation than the criterion equation determined from the data obtained from a numerical experiment by the CFD method.

A cause may be that the CFD model of natural turbulence captures only one shape of the flow field above the pipes (an image of current distribution of flow and thermal field). These fields are markedly non-stationary especially in the upper part of the bundle and change their shape so that the CFD method does not catch their average parameters in time. When measuring determining parameters, the temperatures of surfaces and air are naturally averaged in time due to thermal accumulation of pipes and sensors. Further averaging can be achieved through processing a greater number of data recorded by the central measuring station to a table process.

Comparing the criterion equation for heat transfer in natural convection on an individual horizontal pipe proposed according to Michejv in the form

\[ Nu_i = 0.5(Gr \cdot Pr)^{0.25} \cdot (Pr_i/Pr)^{0.25} \]

for \( 10^3 < Gr \cdot Pr < 10^6 \),

\( (10) \)

For the constant \( b_0 \), regression coefficients \( b_1 - b_4 \), standard deviation \( \sigma \) and correlation index \( R \) following values hold:

\[
\begin{array}{cccccc}
    b_0 & b_1 & b_2 & b_3 & b_4 & R \quad S \\
    4.705 & 0.14 & -0.02 & -0.03 & -29 & 0.958 & 0.0117 \\
\end{array}
\]

Figures 9a - 9d show comparison of values of the Nusselt number computed according to the obtained equation (9) with the values computed from measured results for individual bundles of pipes.
The obtained forms of criterion equation are significantly simpler than equations with polynomial corrections at a good approximation of the Nusselt number determined from experimental measurements.

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